MARKED UP VERSION OF AMENDED CLAIMS

2. (Amended) The method [Method according to] of claim 1, in which use is made of feedstocks ranging from those having an initial boiling point of about ambient to those having a final boiling point of about 650 °C.

3. (Amended) The method [Method according to] of claim 2, in which use is made of feedstocks having a boiling point range such that their 90% boiling point lies in the range between about 400°C and ab out 600 °C.

4. (Amended) The method [Method according to one or more] of claim[s] 1[-3], in which use is made of feedstocks having a sulphur content of not more than 5 %wt [, preferably below 3 %wt].

5. (Amended) The method [Method according to one or more] of claim[s] 1[-4], in which a hydrocarbonaceous feedstock is used containing between about 5 %wt and about 40 %wt of material having a boiling point range which is the same as or higher than the boiling point range of the hydroprocessed product to be produced.

6. (Amended) The method [Method according to] of claim 5, in which the feedstock contains between about 5 %wt and about 40 %wt of material having a boiling point above the final boiling point of the hydroprocessed product.

7. (Amended) The method [Method according to one or more] of claim[s] 1[-6], in which kerosene and/or gas oil are recovered as hydroprocessed product(s) from the hydrotreated feedstock.

8. (Amended) The method [Method according to one or more] of claim[s] 1[-7], in which part or all of the non-recovered material from the treatment with hydrogen is subjected to a catalytic oxidation process which produces hydrogen and carbon (di) oxide.

9. (Amended) The method [Method according to] of claim 8, in which the catalytic oxidation process comprises a catalytic partial oxidation process [and a watergas-shift process].

10. (Amended) The method [Method according to] of claim 8 [or 9], in which hydrogen not used in the hydrotreatment step is used at least partially to produce electricity by feeding it to a fuel cell which is operated to deliver electricity and water (steam).

11. (Amended) The method [Method according to] of claim 10, in which the electricity in excess of that needed for the utilities of the process is produced from excess hydrogen.

12. (Amended) The method [Method according to] of claim 10, in which at least part of the steam needed in the hydrogen manufacturing unit is provided by the fuel cell.

13. (Amended) The method [Method according to one or more] of claim[s] 1 [-12], in which kerosene and/or gas oil, [hydrogen, carbon dioxide and electricity] are produced from no feedstocks other than the hydrocarbonaceous feedstock and water used in the watergas-shift step.

14. (Amended) The method [Method according to one or more] of claim[s] 1[-13], in which hydrogen sulphide generated by the treatment with hydrogen is converted into elemental sulphur by conventional means.

15. (Amended) The method [Method according to one or more] of claim[s] 1[-14], in which use is made of a catalyst system capable of converting at least about 50 %wt per pass[, preferably at least 65 %wt] of the material, having a boiling point range which is the same or above the boiling point range of the hydroprocessed product.

16. (Amended) The method [Method according to] of claim 15, in which use is made of a catalyst containing zeolite beta as active component in the treatment with hydrogen.

17. (Amended) The method [Method according to] of claim 16, in which the zeolite beta-based catalyst is capable of converting at least 90 %wt per pass of the fraction to be treated to obtain the hydroprocessed product.

18. (Amended) The method [Method according to one or more] of claim[s] 15[-17], in which the treatment with hydrogen is carried out at a temperature between about 100 °C and about 550°C[, preferably at a temperature between 250°C and 450°C].

19. (Amended) The method [Method according to one or more] of claim[s] 15[-18], in which the treatment with hydrogen is carried out at a pressure of up to 400 atmospheres[, preferably at a pressure between 10 and 200 atmospheres].

20. (Amended) The method [Method according to one or more] of claim[s] 10[-19], in which the fuel cell step is operated in such a way that it delivers excess electricity.

21. (Amended) The method [Method according to one or more] of claim[s] 9[-20], in which the catalytic partial oxidation step and the fuel cell step are operated in such a way that they generated the internal needs on hydrogen and electricity for the process.

22. (Amended) The method [Method according to one or more] of claim[s] 9[-21], in which the hydrogen generated by the catalytic partial oxidation step has been produced at least partly from hydrocarbons containing at most 4 carbon atoms present in the hydrocarbonaceous feedstock or as produced during the hydrotreatment step.

23. (Amended) The method [Method according to] of claim 22, in which the feedstock for the catalytic partial oxidation step consists of hydrocarbons having about 4 or less carbon atoms.

24. (Amended) The method [Method according to one or more] of claim[s] 1 [-23], in which hydrogen is separated off from the hydrotreated feedstock and from the hydroprocessed product if the latter is not to be recovered prior to the hydrogen manufacturing step.